

## Answer Sheets for CHE654 Homework Set #4 (100 Points)

**Note:** For all problems, submit a copy of your process flow diagram and a copy of your input summary of the process.

**27. (20 points) Quick Property Analysis, I**

Answer the following questions:

(a) The values of the retrieved binary parameters in °C for the 3 binary systems are

Binary System	Interaction Parameters	Range of Temperature (°C)
Acetonitrile-Water		
Ethanol-Butylamine		
Acid-Pyridine		

If a pair has no interaction parameters, why?

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(b) Description of a minimum-boiling azeotrope:

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Description of a maximum-boiling azeotrope:

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Classification:

Acetonitrile-Water :  Minimum  Maximum boiling-point azeotrope

Ethanol-Butyl-amine :  Minimum  Maximum boiling-point azeotrope Acetic

acid-Pyridine :  Minimum  Maximum boiling-point azeotrope

(c) UNIQU-RK property method is not appropriate for the Acetic acid-Pyridine system

because \_\_\_\_\_

Two alternate property methods better suited to predict the azeotrope for the acetic acid-pyridine system are: \_\_\_\_\_

(d) Don't forget to submit the  $T$ - $xy$  plots of each system!

Summary Table:

Binary System	Azeo. Temp.	% Err.	Azeo. X	% Err.
Acetonitrile-Water				
Ethanol-Butylamine				
Acetic acid-Pyridine				

(e) Don't forget to submit the vapor pressure profile (in psia) of all components as a function of  $T$  from 0 to 100 °C.

Rearrange the relative volatility in increasing order:

\_\_\_\_\_

### 29. (20 points) *Choosing Appropriate Property Methods, I*

(a) Activity coefficient  $\gamma$  of ethanol in an equimolar liquid solution of ethanol and cyclohexane at 60 °F and 20 psia.

Property Method: \_\_\_\_\_ O With O Without Henry's Law

Activity coefficient of ethanol = \_\_\_\_\_

- (b) Critical temperature of a mixture with a composition of 30 mol% benzene, 30 mol% cyclohexane, 30 mol% *n*-hexane, and 10 mol% N<sub>2</sub>.

Property Method: \_\_\_\_\_ O With O Without Henry's Law

Critical temperature of the mixture = \_\_\_\_\_ °C

- (c) Vapor fugacity coefficient  $\phi^f$  of formic-acid in an equimolar mixture of formic-acid and water at 20 psia in which 50 mol% of the mixture is vapor.

Property Method: \_\_\_\_\_ O With O Without Henry's Law

Vapor fugacity coefficient of formic-acid = \_\_\_\_\_

- (d) Which gas has higher solubility in the liquid solution and by how much: 1 lbmol of helium or 1 lbmol of argon in a liquid solution of 10 lbmol of ethanol at 70 °F and 14.7 psia? (Special note: you are not allowed to pick an equation of state for this problem).

Property Method: \_\_\_\_\_ O With O Without Henry's Law

Gas with higher solubility is \_\_\_\_\_ and by more than \_\_\_\_\_ ppm (mole)

- (e) Energy required to vaporize 1 gmol (i.e. heat of vaporization) of a saturated liquid containing 40 mol% aniline, 40 mol% acetol, and 20 mol% cyclohexene at 1 bar.

Property Method: \_\_\_\_\_ O With O Without Henry's Law

Energy required = \_\_\_\_\_ cal

- (f) Vapor compressibility factor  $Z$  of a mixture containing 40 mol% formaldehyde, 40 mol% chloroform, and 20 mol% acetylene at 150 °C and 20 bar.

Property Method: \_\_\_\_\_ O With O Without Henry's Law

Vapor compressibility factor = \_\_\_\_\_

- (g) Solubility of water in the organic phase in a mixture containing 45 mol% water, 45 mol% 1-methylcyclohexanol, and 10 mol% O<sub>2</sub> at 20 °C and 1 bar.

Property Method: \_\_\_\_\_ O With O Without Henry's Law

Solubility of water = \_\_\_\_\_ mol%

- (h) What temperature increase is required to produce a vapor stream containing 30 mol% acetone from a one-lbmole saturated liquid mixture with an overall composition of 40 mol% water, 40 mol% benzene, and 20 mol% acetone at 14.7 psia, assuming there is no pressure change in the vaporization? (You must save this problem and email the file to me at the end of the exam.)

Property Method: \_\_\_\_\_ O With O Without Henry's Law

Temperature increase = \_\_\_\_\_ °F

**30. (20 points) *Choosing Appropriate Property Methods, II***

- (a) Which of the following 3 components has the lowest volatility at  $T = 80$  °F: cyclobutane, 1,2-butadiene, or ethyl-chloride?

Property Method: \_\_\_\_\_ O With O Without Henry's Law

Component with the lowest volatility = \_\_\_\_\_

- (b) The K-value of ethanol in a binary mixed-phase (30 mole% vapor) mixture of 50 mole% water and 50 mole% ethanol at 200 psia.

Property Method: \_\_\_\_\_ O With O Without Henry's Law

K-value of ethanol = \_\_\_\_\_

- (c) Solubility (mole ppm) of CO<sub>2</sub> in water in a mixture of 20 mole% CO<sub>2</sub> and 80 mole% water at 5 psia and 80 °C.

Property Method: \_\_\_\_\_ O With O Without Henry's Law

Solubility of CO<sub>2</sub> = \_\_\_\_\_ ppm

- (d) Solubilities (mole%) of acetic-acetone in the aqueous phase and alcohol phase of a mixture of 20 mole% *n*-butanol, 20 mole% acetone, and 60 mole% water at 14.7 psia and 50 °F.

Property Method: \_\_\_\_\_ O With O Without Henry's Law

Solubility in aqueous phase = \_\_\_\_\_ %; Solubility in alcohol phase = \_\_\_\_\_ %

- (e) Heat of mixing (excess enthalpy) when 1 lbmol of acetol is mixed with 1 lbmol of acetonitrile at 20 psia and 100 °F.

Property Method: \_\_\_\_\_ O With O Without Henry's Law

Heat of mixing = \_\_\_\_\_ Btu/lbmol

- (f) Vapor fugacity coefficient of acetic-acid in a vapor-liquid mixture (with 30 mole% vapor) containing 30 mole% acetic-acid, 30 mole% acetone, and 40 mole% ethanol at 20 psia.

Property Method: \_\_\_\_\_ O With O Without Henry's Law

Vapor fugacity coefficient of acid = \_\_\_\_\_

- (g) Bubble-point pressure of a mixture of 30 mole% *n*-pentane, 30 mole% benzene, and 40 mole% cyclohexane at 30 °C.

Property Method: \_\_\_\_\_ O With O Without Henry's Law

$P_{\text{BUBBLE}} =$  \_\_\_\_\_ bar

**32. (20 points) Waste Stream Purification Using Multiple Property Methods**

- (a) SR-POLAR property method is appropriate for the high pressure section of the process because

\_\_\_\_\_  
\_\_\_\_\_

Suitable method for the LP section: \_\_\_\_\_

- (b) Don't forget to submit input summary!

Molar vapor fraction in the LP-partial condenser: \_\_\_\_\_

Operating parameters of the 2 columns:

	<u>Reflux ratio</u>	<u>Actual # of stages</u>
LP-Column	_____	_____
HP-Column	_____	_____

Mole fractions of acetone, water, and acetic acid in their respective purified streams:

Acetone from LP-column: \_\_\_\_\_

Water from HP-column: \_\_\_\_\_

Acetic acid from HP-column: \_\_\_\_\_

**33. (20 points) Toluene-Benzene Recovery Process with Multiple Property Methods**

- (a) Mole fraction of benzene in the 2nd-Column overhead stream: \_\_\_\_\_

Molar ratio toluene: hydrogen in reactor feed: \_\_\_\_\_

- (b) Hydrogen molar feed flow rate: \_\_\_\_\_ gmol/min

Mole fraction of benzene in the 2nd-Column overhead stream: \_\_\_\_\_